

Benchmarking a Novel 0-D Model Against Data from Two-Fluid Model Simulations of a Wet Fluidized Bed

Stefan Radl, Mohammadsadeqh Salehi

Institute of Process and Particle Engineering, Graz University of Technology

Maryam Askarishahi

Research Center Pharmaceutical Engineering GmbH, Graz

radl@tugraz.at

LoD

0.0178

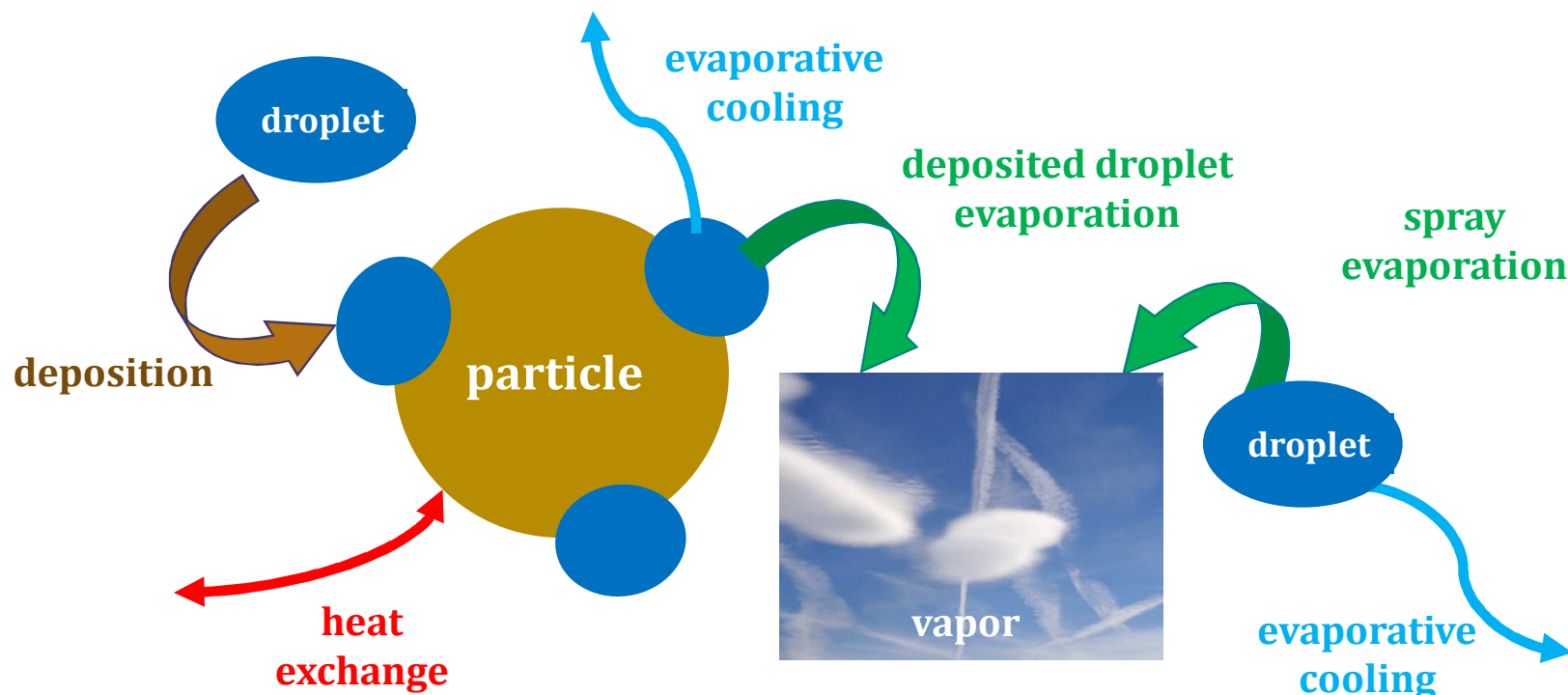
0.0175

0.0172

0.0168



Phenomena governing wet fluidized beds (WFBs)



<https://www.glatt.com>

Askarishahi et al. (2017), AIChE Journal, 63:2569-2587

Askarishahi (2018). PhD thesis, TU Graz.

<https://github.com/CFDEMproject>

Motivation

developing a toolset (CFD-DEM/TFM/0D) to predict WFB performance

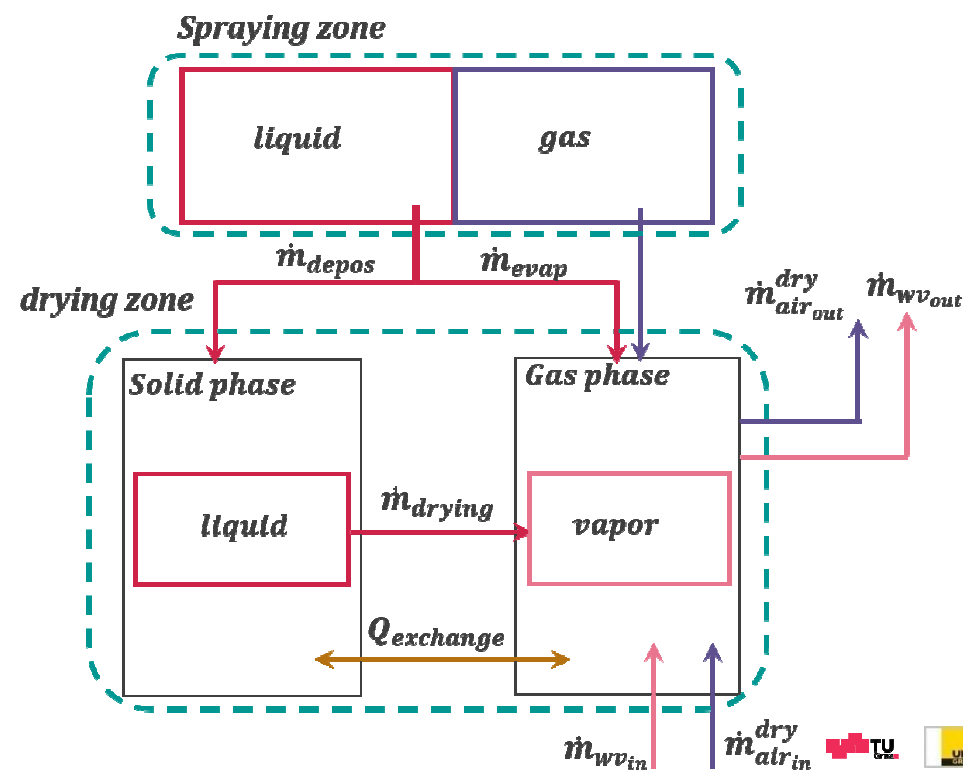
Euler-Euler-Euler Approach
Two-Fluid Model (CFD-TFM)

Compartment (0D) model



Multiphase Flow with
Interphase eXchanges

<https://mfix.netl.doe.gov>



Model implementation mass balance for **water (liquid)**

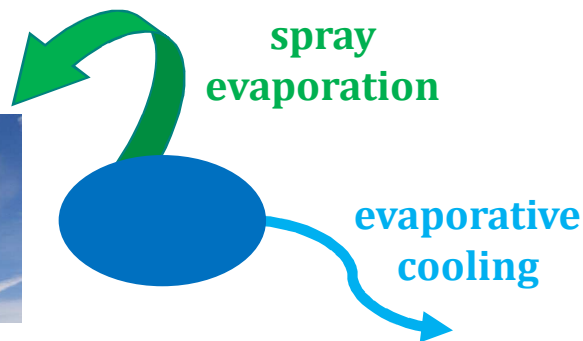
+ standard models for continuity, momentum & heat,
KTGF + μ -I rheology, Schneiderbauer stress BCs

$$\underbrace{\frac{\partial}{\partial t}(\varepsilon_g \rho_g x_{wl})}_{\text{Accumulation}} + \underbrace{\nabla \cdot (\varepsilon_g \rho_g x_{wl} \mathbf{u}_g)}_{\text{Convection}} = \underbrace{\nabla \cdot (D_{gn} \nabla \varepsilon_g \rho_g x_{wl})}_{\text{Dispersion}} + \underbrace{\dot{S}_{\text{spray}}}_{\text{Source}} \underbrace{[-\dot{S}_{\text{evap}} - \dot{S}_{\text{depos}}]}_{\text{Sinks}}$$

Droplet evaporation

$$\dot{S}_{\text{evap}} = (\rho_{w,\text{sat}} - \rho_f \mu_{wv}) a_d \beta_d \varepsilon_d$$

μ_{wv} : vapor mass loading
 $\rho_{w,\text{sat}}$: saturation density
 ε_d : droplet volume fraction
 β_d : mass transfer coeff.
 a_d : sepcific surface area

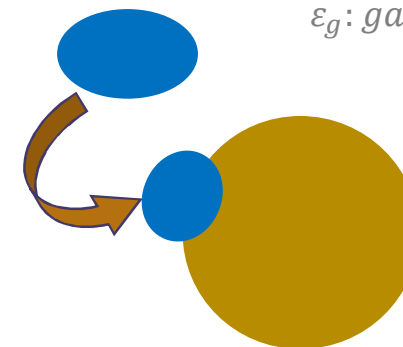


Droplet deposition

$$\dot{S}_{\text{depos}} = -\lambda |\mathbf{u}_d - \mathbf{u}_p| \mu_{wl} \varepsilon_g \rho_g$$

λ : Filtration coefficient after Kolakaluri's Model

μ_{wl} : liquid mass loading
 ε_g : gas volume fraction



Model implementation

mass balance for **water vapor**

$$\underbrace{\frac{\partial}{\partial t}(\varepsilon_g \rho_g x_{wv})}_{\text{Accumulation}} + \underbrace{\nabla \cdot (\varepsilon_g \rho_g x_{wv} \mathbf{u}_g)}_{\text{Convection}} = \underbrace{\nabla \cdot (D_{gn} \nabla \varepsilon_g \rho_g x_{wv})}_{\text{Diffusion/Dispersion}} + \underbrace{\dot{S}_{dry} + \dot{S}_{evap}}_{\text{Sources}}$$

Particle drying

$$\dot{S}_{dry} = (\rho_{w,sat} - \rho_g \mu_{wv}) a_p \psi_{liq} \beta_p \varepsilon_s$$

ψ_{liq} : Particle surface coverage after Kariuki's Model

$$\psi_{liq} = 1 - [1 - f]^{\Phi_p / f}$$

μ_{wv} : vapor mass loading

$\rho_{w,sat}$: saturation density

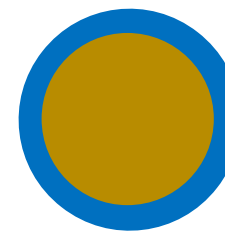
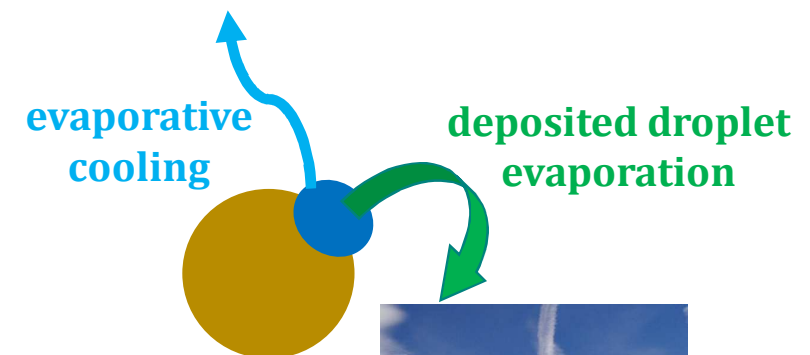
φ_d : droplet volume fraction

β_p : mass transfer coeff.

a_p : specific surface area

f : droplet foot print area

Φ_p : coating number



Continuous film, $\psi_{liq} = 1$

CFD-TFM

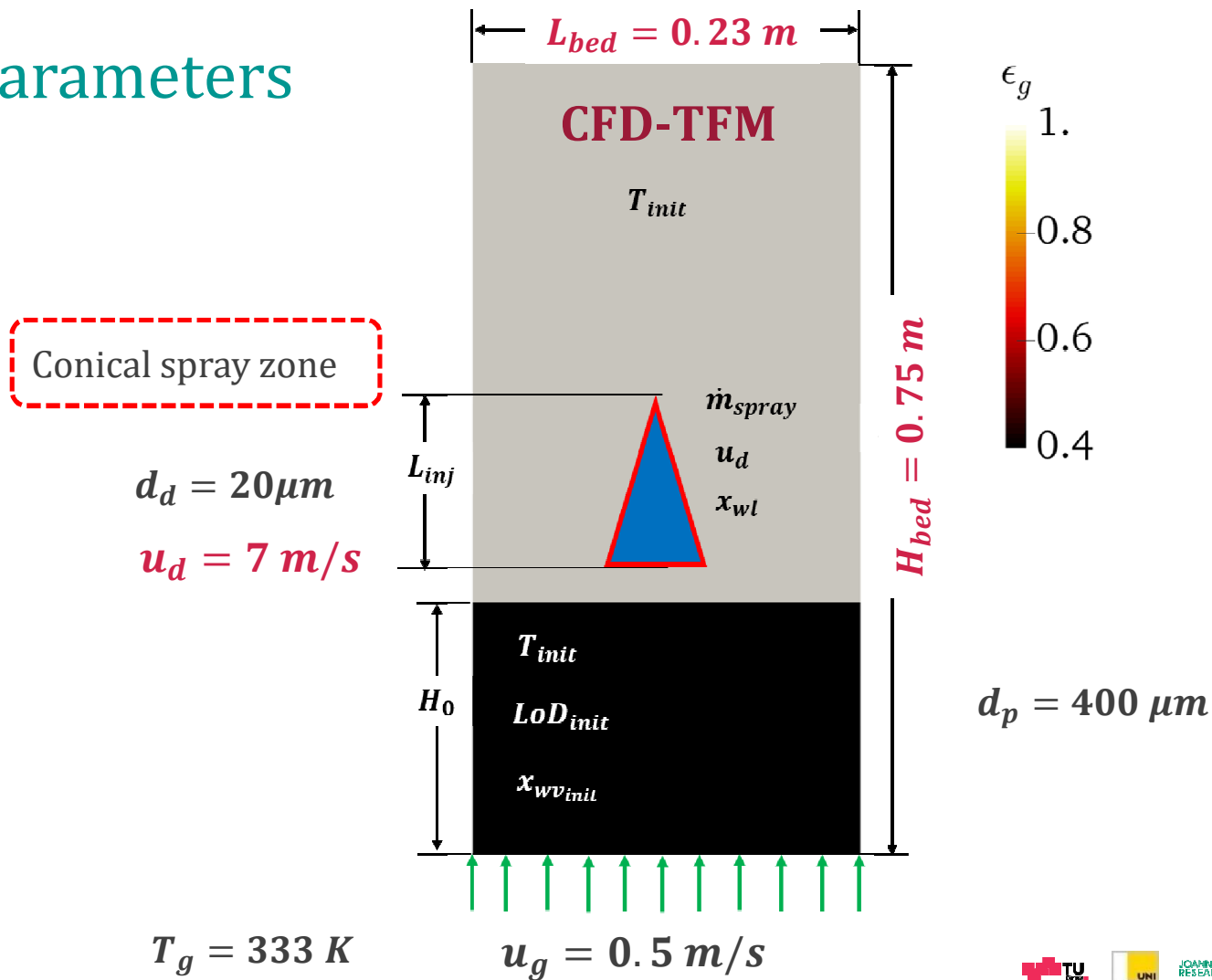
fluidized bed
performance assessment

CFD-TFM simulation

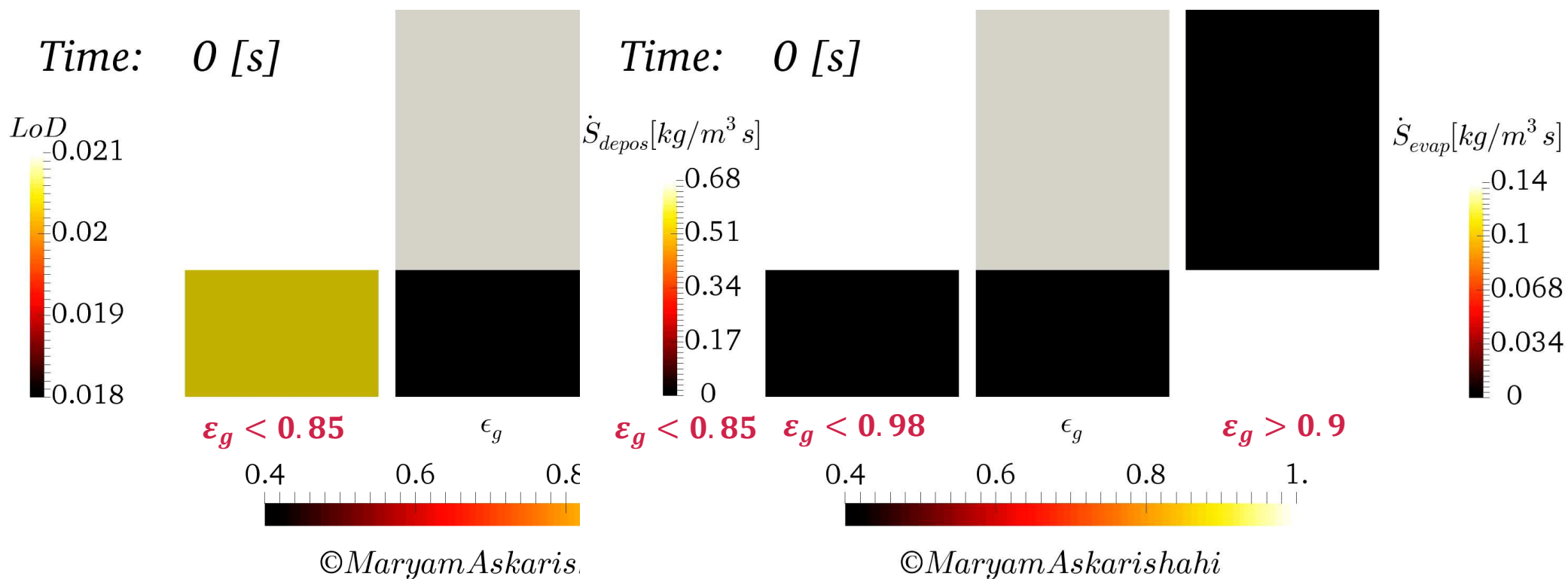
Setup and operating parameters



<https://www.glatt.com>



Qualitative performance of WFB



CFD-TFM

the degree
of uniformity

Uniformity of bed

How to assess?

Is it possible to represent the bed *performance* with the *single values*?

Temperature | *LoD* | *vapor content*

How uniform is the distribution in the bed?

Qualitative

The time-averaged *contour-plots* for the *exchange rates* and the *flow properties*

Quantitative

The *uniformity degree* through LoD and temperature *standard deviation*

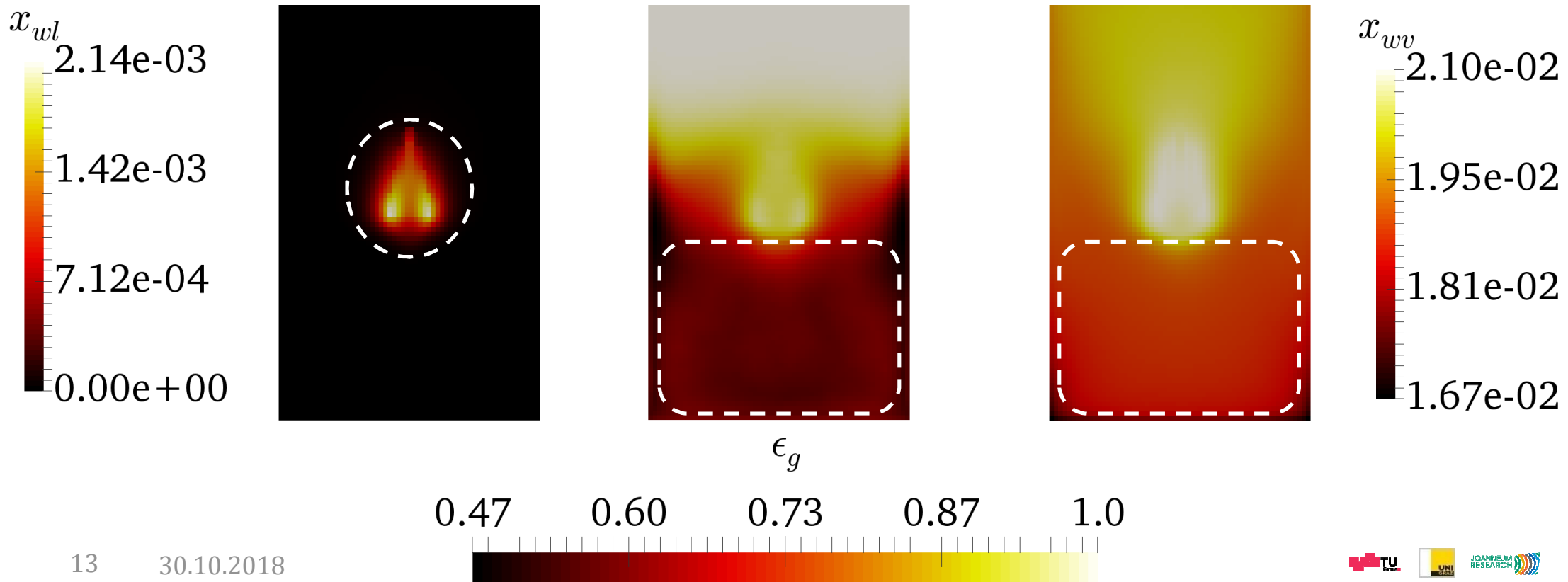
Uniformity degree: **Qualitative** examination

Time-averaged flow property distribution

droplet mass fraction

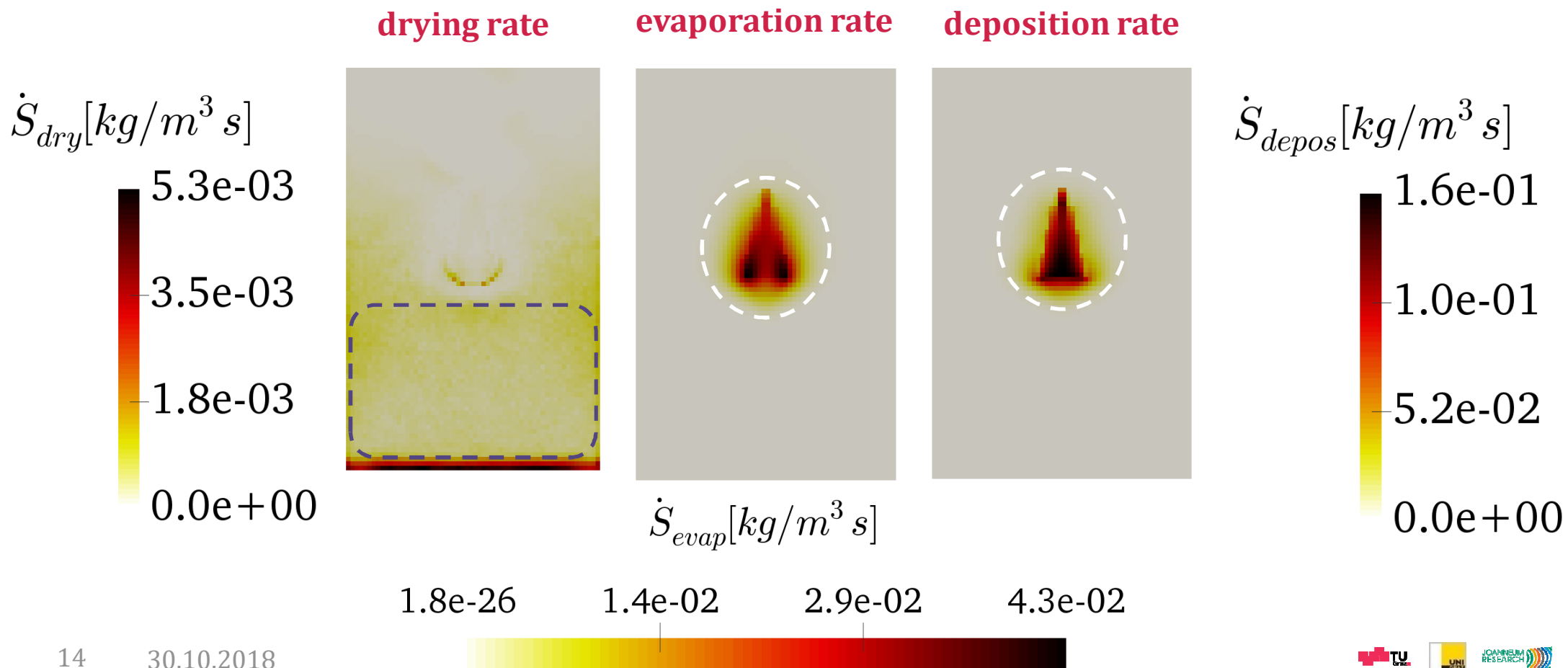
bed voidage

vapor mass fraction



Uniformity degree: **Qualitative** examination

Time-averaged exchange rate distribution

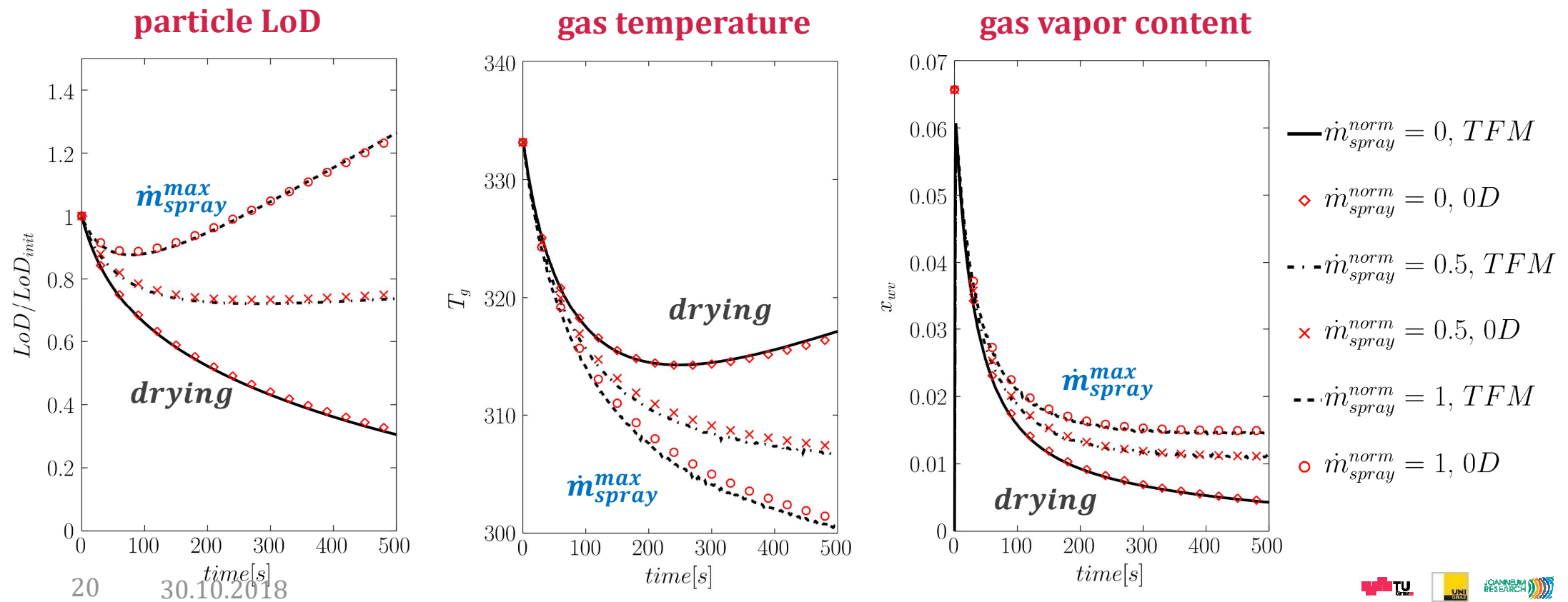


CFD-TFM versus 0D model

0D model validity against TFM approach

effect of spray rate

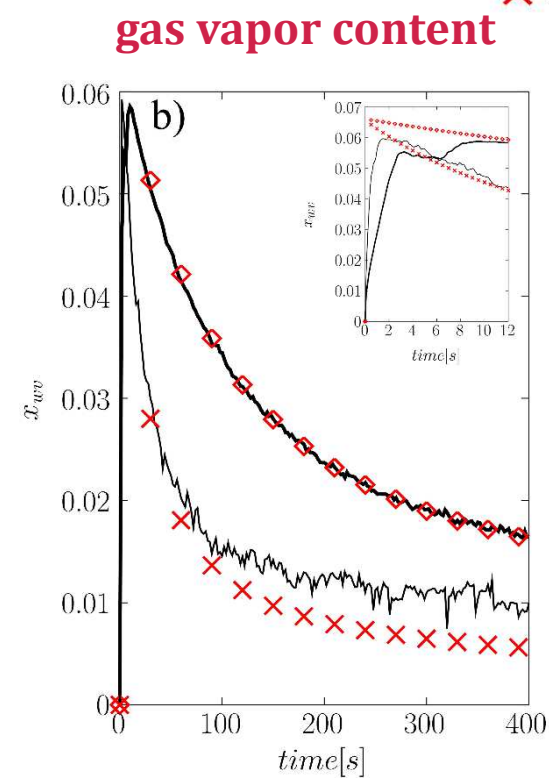
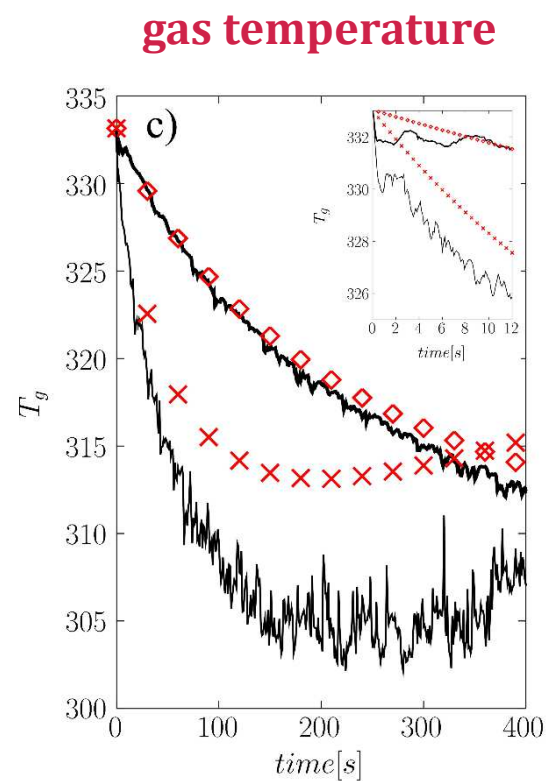
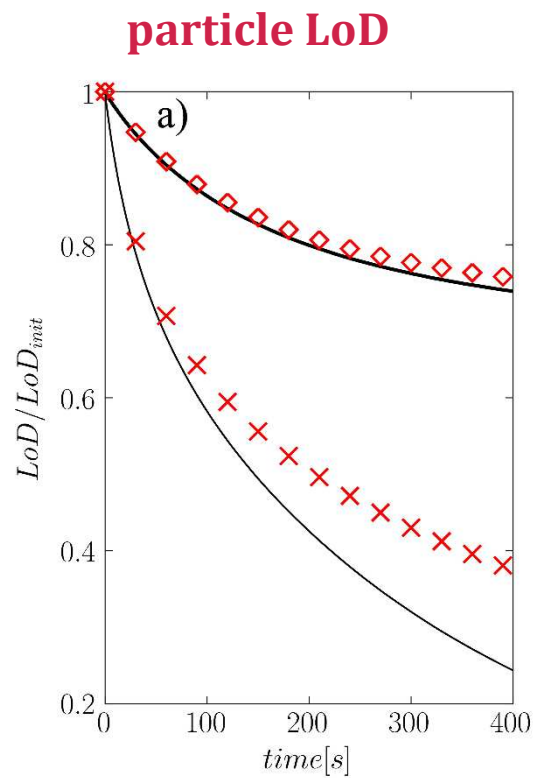
$\dot{m}_{\text{spray}}^{\text{norm}}$ is defined as the ratio of spray rate to the maximum spray rate ($RH_{\text{out}} = 100\%$)



0D model validity against TFM approach effect of spray rate

Effect of bed aspect ratio

- $H_0/L_{bed} = 0.65$, TFM
- ◇ $H_0/L_{bed} = 0.65$, 0D
- $H_0/L_{bed} = 0.15$, TFM
- × $H_0/L_{bed} = 0.15$, 0D



Conclusions and outlooks

Development of a **0D model** based on the results of **TFM simulation**

Formation of two **phenomenon-specific zones**

Quantification of **“well-mixed-ness”** via the **degree of uniformity** for LoD and temperature

demonstration of the 0D model validity on fulfilling the criteria for **“well-mixed” condition**

Validation and integration of **cohesion** comes next



**Thank you for your
attention!**

Open PhD Positions for „MATHGram“

- **Topic: particles + heat**
- **Lead: Prof. Charley Wu (Univ. Surrey)**
- **15 PhDs across Europe**
- **Starts 2019**
- **2 PhDs in wonderful Austria (Graz/Linz/Vienna)**
- **Apply now! (ippt.turaz.at/jobs, cfdem.com)**

<https://www.graztourismus.at>



Benchmarking a Novel 0-D Model Against Data from Two-Fluid Model Simulations of a Wet Fluidized Bed

Stefan Radl, Mohammadsadeqh Salehi

Institute of Process and Particle Engineering, Graz University of Technology

Maryam Askarishahi

Research Center Pharmaceutical Engineering GmbH, Graz

radl@tugraz.at

LoD

0.0178

0.0175

0.0172

0.0168

